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Evaluation of a multiphase LB model for coating flows

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What are coating flows?







- Can categorize as either natural wetting or forced wetting
 - -Droplet spreading \rightarrow natural wetting
 - -Coating flows \rightarrow forced wetting
- Central to wetting is the problem of the moving contact-line



In first part of talk gas will be neglected – modelling only includes liquid



Problems with continuum modelling



- Presence of a finite contact angle causes problems
- Boundary conditions on liquid-gas and solid-liquid interfaces are in conflict at the contact line
- Contact line is stationary, but boundary is moving
- Shear stress is infinite
- Usually have to prescribe contact angle and slip (relieve stress)





Problems With Slip Models





- 'Rolling' motion observed in experiments
- Particle on liquid-gas interface passes through contact line and onto solid-liquid interface
- 'Sliding' motion produced by most slip models
- Particle on liquid-gas interface never reaches contact line TSI because $u \rightarrow 0$

Problems With Slip Models





- Coating flows driven at high speed often have large θ_d
- Slip region produces obstacle-type flow
- Pressure is singular





Based on idea of relaxation of surface tension

–Interfacial tension changes smoothly from L-G to L-S

-Near contact line interfacial tensions deviate from equilibrium values

-Force balance at contact line gives contact angle as function of flow

- The usual kinematic and impermeability conditions are replaced with equations describing fluxes between the bulk and the interfaces
- The stress conditions are modified to account for variable interfacial tensions
- Liquid velocity at the contact line is not zero it is determined as part of the solution. Rolling motion preserved.
- Dynamic contact angle is obtained from solution



`Interface Formation Model' of Shikhmurzaev



- Model has been used successfully for Stokes flows
 - –Lukyanov & Shikhmurzaev (2007) Phys. Rev. E 75, 051604
 - -considered a microfluidic curtain coater
 - –observed variation of θ_d with a number of flow parameters
 - -used a combined finite element-boundary integral element method
- Navier-Stokes finite element solutions for the full-scale curtain coater are now possible.
- But, air-entrainment predictions are not possible.



- Supported by molecular dynamics simulations, a diffuse interface for the liquid-gas, solid-liquid and solid-gas is more amenable to varying interfacial density.
- Diffuse interfaces can rupture and so could help to predict the important aspect of wetting failure, i.e. air-entrainment.
- Several multiphase lattice Boltzmann (LB) approaches exist.
- Wetting line tests for an LB method are:
 - 1. Forced wetting with failure
 - 2. Wetting line hysteresis
 - 3. Natural wetting (spreading/sticking) [agreement with experiments]





- Based on work of He, Chen & Zhang (1999)
- Use mean-field approximation for intermolecular attractions, and include an exclusion volume effect to...
- Rework force term in Boltzmann equation into a surface tension force
- Use **non-ideal equation of state** to achieve phase separation
- Introduce an **index function**, ϕ , to track the interface between two phases
- Results in a diffuse interface model
 - index function, and fluid density, changes smoothly but rapidly between phases



Finite-density Multiphase Lattice Boltzmann Equations



Following He, Chen and Zhang, two LB equations with forcing are derived for f_i and g_i, the moments of which give the macroscopic properties; mass and momentum densities, and pressure respectively as

$$\boldsymbol{\phi}(\boldsymbol{x}_{\alpha},t) = \sum f_{i}(\boldsymbol{x}_{\alpha},t) \quad (\boldsymbol{\phi} \text{ tracks density} = \text{index function})$$

$$\rho u_{\alpha}(\boldsymbol{x}_{\alpha},t) = \frac{1}{RT} \sum e_{i\alpha} g_{i}(\boldsymbol{x}_{\alpha},t) + \frac{1}{2} \left[\kappa \rho \frac{\partial}{\partial \boldsymbol{x}_{\alpha}} (\nabla^{2} \rho) + B_{\alpha} \right] \delta t$$

$$p(\boldsymbol{x}_{\alpha},t) = \sum g_{i}(\boldsymbol{x}_{\alpha},t) - \frac{1}{2} u_{\alpha} \frac{\partial \psi(\rho)}{\partial \boldsymbol{x}_{\alpha}} \delta t$$



Finite-density Multiphase Lattice Boltzmann Equations



- Model is for a liquid and its gas. Values of the index function for liquid, φ_L , and gas, φ_G are obtained from the EoS and Maxwell's equal area construct.
- The liquid and gas values of φ can be used to account for the different fluid properties between the phases, that is

$$\rho(\boldsymbol{\phi}) = \rho_G + \frac{\boldsymbol{\phi} - \boldsymbol{\phi}_G}{\boldsymbol{\phi}_L - \boldsymbol{\phi}_G} (\rho_L - \rho_G)$$

- The same is true for the viscosity, μ.
- Can be applied with MRT (see Premnath and Abraham (2007))



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Wetting

Use the approach of Iwahara et al. (2003)

Define a **surface affinity** – a normalised surface density

$$\alpha_s = \frac{\phi - \phi}{\phi_L - \overline{\phi}}$$
, where $\{\overline{\phi} = (\phi_L + \phi_G)/2i\}$

A planar interface has the profile (Rowlinson & Widom 1982)

$$\boldsymbol{\phi}(z) = \overline{\boldsymbol{\phi}} - \frac{1}{2}(\boldsymbol{\phi}_L - \boldsymbol{\phi}_G) \tanh\left(\frac{z - z_0}{\delta}\right)$$

The liquid-gas surface tension is therefore

$$\sigma_{LG} = \kappa \int_{-\infty}^{\infty} \left(\frac{\partial \phi}{\partial z} \right)^2 dz = \frac{\kappa (\phi_L - \phi_G)^2}{4\delta} \int_{-1}^{1} (1 - \alpha^2) d\alpha$$
$$\frac{\kappa (\phi_L - \phi_G)^2}{3\delta}$$



Similar expressions for the solid-liquid and solid-vapour surface tensions substituted into Young's equation give

$$\cos\theta_S = \alpha_S (3 - \alpha_S^2)/2$$

Static contact angle can be specified via the surface affinity

Index-function density at boundary given by

$$\varphi = \overline{\phi} + (\phi_L - \overline{\phi}) \alpha_S, \quad \{ \overline{\phi} = \frac{1}{2} (\phi_L + \phi_G), \quad -1 \le \alpha_S \le 1 \overline{i}$$







- Two-phase cavity
- Solid walls





Static Case – Interface Shape





Static Case – Contact Angle



Angle of interface matches imposed angle at roughly 7 lattice units away from the boundary

Just outside the diffuse three-phase contact region

Use this as the point to measure variation in contact angle













Contact Angle Versus Speed





Combustion Tribology Thin Films Corrosion

Dynamic Case – Young Equation





Dynamic Case – Surface Tension





Dynamic Case – Surface Energy





Dynamic Case – Surface Energy







Test Problem 2 (Wetting line hysteresis)

u>0

u=0

u<0



uniform wettability



sinusoidally varying wettability



Test Problem 2 (Wetting line hysteresis)





Test Problem 3 (Natural wetting spreading/sticking)



- Flow of a droplet down an incline with a sinusoidally varying wettability of wavelength A
- Varying A for fixed interface thickness
- Droplet is pinned for certain values



A Tale of Two Length Scales

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- What is the effect of interface thickness for wetting of non-uniform surfaces?
 - interface thickness versus characteristic size of non-uniformity
- Interface thickness is always ~4 or 5 lattice units...can scale up problem
- Use two lattices one twice the size of the other (i.e. twice as dense)
 - need to adjust relaxation time and surface tension parameter to match physical scales on each lattice
- Use sinusoidal/alternating surface affinity





Motion of slug centre





Motion of slug centre





- Density ratio limited
 - several models now available addressing this issue, though wetting is still an issue for many
- Issues with the surface tension and surface energies.
 - Calculations of surface tension/energy via the thermodynamic (Cahn) approach is for static conditions, can we define a "mechanical" approach for the dynamic situation.
- Wetting models for moving rough boundaries needed
 - interface thickness a key factor



Conclusions



- Able to capture qualitatively many wetting phenomena (static contact angle, forced wetting to failure, contact line hysteresis and natural wetting to the point of sticking on a non-uniform surface)
- Simple model and algorithm only one wetting parameter
- Care needed in understanding effect of interface thickness (as this will dictate the length scale?)
- Work needed to make quantitatively accurate (is the thermodynamic description of surface energy sufficient?)

