



Lattice Boltzmann schemes for the *Brinkman equation* in extremely heterogeneous porous media: bulk, boundary, interface

Gonçalo Silva & Irina Ginzburg

Groupe de travail “Schémas de Boltzmann sur réseau”

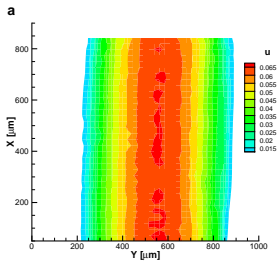
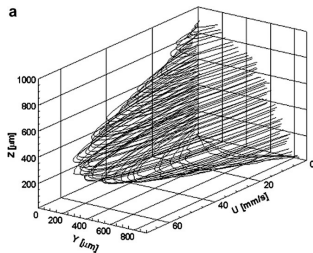
6th May 2015

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 - Boundary/interface
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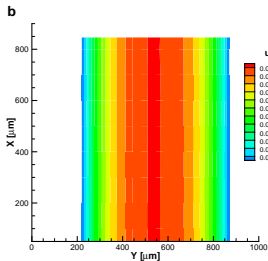
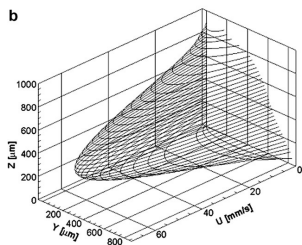
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Experiments

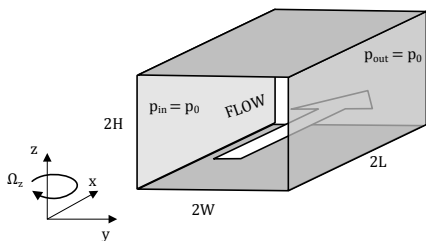
Micro-PIV



CFD

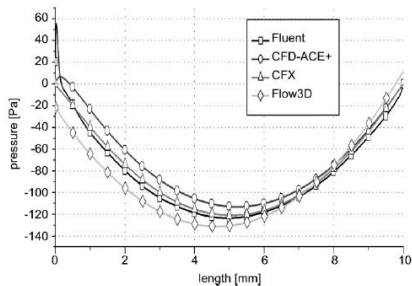


A simple numerical verification test



Centrifugal-driven rotating channel

flow setup



Streamwise pressure solution
predicted by several commercial CFD codes

– *image source: Glatzela et al. 2008*

LBM studies:

Physica A 390 (2011) 1065–1095



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A study on the inclusion of body forces in the lattice Boltzmann BGK equation to recover steady-state hydrodynamics

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First- and second-order forcing expansions in a lattice Boltzmann method reproducing isothermal hydrodynamics in artificial compressibility form

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Truncation errors and the rotational invariance of three-dimensional lattice models in the lattice Boltzmann method

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Heterogeneous porous media systems

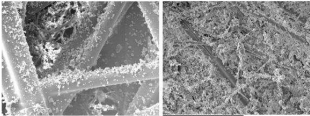


Figure 1: SEM (Scanning Electron Microscope) view of used cabin air filter

Figure 3: SEM of dust-laden fiber has passed the depth filtration stage (Transition stage)

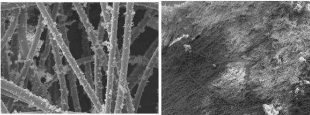


Figure 2: SEM representing the stationary stage of dust loading

Figure 4: SEM of dust cake formation on the fiber surface

image source: www.ntu.edu.sg

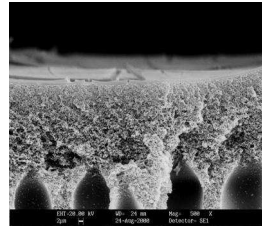


image source: www.memfil.com

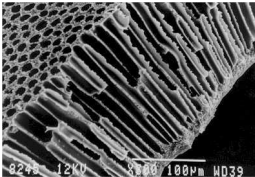


image source: www.ntu.edu.sg

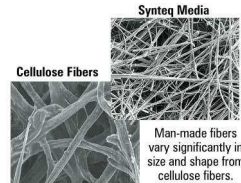


Figure 2. Liquid Filtration Media

Governing equations (nondimensional)

Stokes-Brinkman-Darcy equations

$$\vec{\nabla} \cdot \vec{u} = 0$$

$$f(\phi) \vec{\nabla} p = \Delta \vec{u} - \sigma^2 \vec{u}$$

subject to proper interface/solid BC.

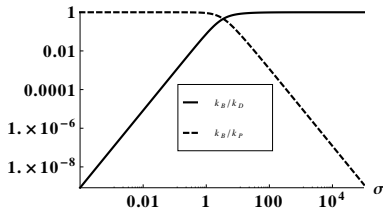
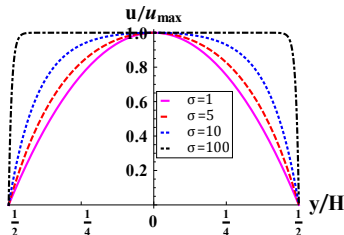
Solution is controlled by:

- $f(\phi)$ (herein = 1, for simplicity)
- $\sigma^2 = f(\phi) H^2/k$

Given $\sigma \Rightarrow$ **3** dynamical regimes follow:

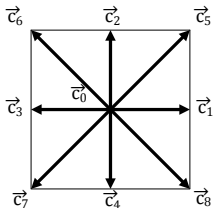
- ① $\sigma < 1$: “Open” flow \rightarrow Stokes
- ② $\sigma \sim 1$: “Interface” flow \rightarrow Brinkman
- ③ $\sigma > 1$: “Constant” flow \rightarrow Darcy

Channel flow solutions:



D2Q9

LB evolution equation:



$$\textcircled{1} \text{ Streaming: } f_q(\vec{r} + \vec{c}_q, t + 1) = \tilde{f}_q(\vec{r}, t)$$

$$\textcircled{2} \text{ TRT collision:}$$

$$\tilde{f}_q(\vec{r}, t) = f_q(\vec{r}, t) + g_q^+ + g_q^-$$

where $g_q^\pm = -s^\pm (f_q^\pm - e_q^\pm)$ defined by:

- Symmetric equilibrium $e_q^+ = t_q P(\rho)$

- Anti-symmetric equilibrium

$$e_q^- = j_q + \Lambda^- F_q$$

$$\text{with } j_q = t_q(\vec{j} \cdot \vec{c}_q) \text{ and } F_q = t_q(\vec{F} \cdot \vec{c}_q)$$

- Relaxation functions $\Lambda^\pm = \left(\frac{1}{s^\pm} - \frac{1}{2}\right) > 0$
with $s^\pm \in]0, 2[$

- Brinkman viscosity $\nu_B = \frac{\nu}{f(\phi)} = \frac{\Lambda^+}{3}$

D2Q9

LB evolution equation:

③ Conservation:

- Mass $\rho = \sum_{q=0}^{Q-1} f_q$
- Momentum $\rho_0 \vec{u} = \vec{j} = \sum_{q=1}^{Q-1} \vec{c}_q f_q - \frac{1}{2} \vec{F}$

④ Invariance:

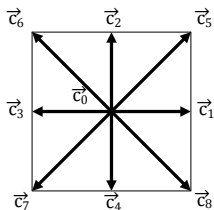
- Steady-state solutions are fixed by $\Lambda = \Lambda^+ \Lambda^-$ (viscosity-independence)

⑤ BF scheme:

- Brinkman force term: $\vec{F} = \vec{F}^p - B_f \vec{j}$
with $B_f = \frac{\nu}{k}$

⑥ IBF scheme:

- Introduce redefine symmetric relaxation function, e.g. $\Lambda_*^+ = \frac{3(4+B)\Lambda^+}{4(3+2B\Lambda)}$
where $B = \frac{\sigma^2}{H^2}$ or $B = \frac{B_f}{\nu_B}$



Steady-state recurrence equations:

- One pair of linear combinations per link:

$$g_q^+ = \bar{\Delta}_q e_q^- - \Lambda^- \bar{\Delta}_q^2 e_q^+ + \left(\Lambda - \frac{1}{4}\right) \bar{\Delta}_q^2 g_q^+$$

$$g_q^- = \bar{\Delta}_q e_q^+ - \Lambda^+ \bar{\Delta}_q^2 e_q^- + \left(\Lambda - \frac{1}{4}\right) \bar{\Delta}_q^2 g_q^-$$

- And another pair per link:

$$\bar{\Delta}_q g_q^- = \bar{\Delta}_q^2 e_q^+ - \Lambda^+ \bar{\Delta}_q^2 g_q^+$$

$$\bar{\Delta}_q g_q^+ = \bar{\Delta}_q^2 e_q^- - \Lambda^- \bar{\Delta}_q^2 g_q^-$$

where first and second central linkwise finite differences are:

- $\bar{\Delta}_q \psi = \frac{1}{2} (\psi(\vec{r} + \vec{c}_q) - \psi(\vec{r} - \vec{c}_q))$
- $\bar{\Delta}_q^2 \psi = \psi(\vec{r} + \vec{c}_q) - 2\psi(\vec{r}) + \psi(\vec{r} - \vec{c}_q)$

General solution:

- Exact steady macroscopic equations:

$$\sum_{q=0}^{Q-1} g_q^+ = 0, \quad \sum_{q=1}^{Q-1} g_q^- \vec{c}_q = \vec{F}$$

- Taking the moments of recurrence equations g_q^\pm :

$$\textcircled{1} \quad \bar{\nabla} \cdot \vec{j} = \Lambda^- \bar{\Delta}^2 P - \left(\Lambda - \frac{1}{4}\right) \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 g_q^+$$

$$\textcircled{2} \quad \bar{\nabla} P - \vec{F} = \frac{\Lambda^+}{3} \bar{\Delta}^2 \vec{j} + \Lambda \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 F_q^- \vec{c}_q - \left(\Lambda - \frac{1}{4}\right) \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 g_q^- \vec{c}_q$$

$$\bullet \quad \bar{\nabla} \cdot \vec{j} = \sum_{q=1}^{Q-1} \bar{\Delta}_q j_q$$

$$\bullet \quad \bar{\Delta}^2 P = \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 P_q$$

$$\bullet \quad \bar{\nabla} P = \sum_{q=1}^{Q-1} \bar{\Delta}_q P_q \vec{c}_q$$

$$\bullet \quad \bar{\Delta}^2 \vec{j} = 3 \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 j_q \vec{c}_q$$

- Isotropic correction
(Brinkman eq.):

$$\Lambda \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 F_q^- \vec{c}_q = -\frac{\Lambda B_f}{3} \bar{\Delta}^2 \vec{j}$$

- Anisotropic correction
(Brinkman eq.):

$$\left(\Lambda - \frac{1}{4}\right) \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 g_q^- \vec{c}_q = ?$$

Channel solution:

Straight/diagonal channel in rotated coordinate system (x', y') :

- ① Momentum: $\sum_{q=1}^{Q-1} g_q^- c_{qx'} = F_{x'}$ \implies $g_q^- = 3t_q F_{x'}(y') c_{qx'} c_{qy'}^2$
- ② Periodic condition: $g_q^- = 0$ if $c_{qy'} = 0$

Anisotropic correction (Brinkman eq.):

$$\left(\Lambda - \frac{1}{4}\right) \sum_{q=1}^{Q-1} \bar{\Delta}_q^2 g_q^- \vec{c}_q = -3 \left(\Lambda - \frac{1}{4}\right) B_f \bar{\Delta}_{y'}^2 j_{x'} \sum_{q=1}^{Q-1} t_q c_{qx'}^2 c_{qy'}^2 = -\left(\Lambda - \frac{1}{4}\right) B_f \bar{\Delta}_{y'}^2 j_{x'}$$

Total correction (Isotropic+Anisotropic):

$$-\frac{\Lambda B_f}{3} \bar{\Delta}_{y'}^2 j_{x'} + \left(\Lambda - \frac{1}{4}\right) B_f \bar{\Delta}_{y'}^2 j_{x'} = B_f \left(\frac{8\Lambda-3}{12}\right) \bar{\Delta}_{y'}^2 j_{x'}$$

Channel solution:

Brinkman forcing modifies effective viscosity of Laplacian term

$$\bar{\nabla}_{x'} P - F_{x'} = \frac{\Lambda^+}{3} \rho_0 (1 + \delta) \bar{\Delta}_{y'}^2 u_{x'}$$

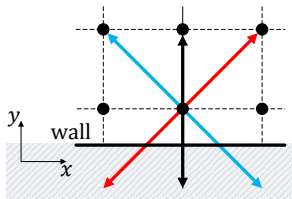
where $\delta = B \left(\frac{8\Lambda - 3}{12} \right)$ with $B = \frac{3B_f}{\Lambda^+}$

Observations:

- Consistency requires viscosity independent solutions.
Impossible for BGK since $\Lambda = \left(\tau - \frac{1}{2} \right)^2$ makes $\delta(B, \nu)!$
- No numerical oscillations require $\delta > -1$,
straight channel: $B < \frac{12}{3-8\Lambda}$.
- Idea of IBF, giving $\Lambda^+ = 3\nu_B$, $B_f = \nu/k$ and Λ , redefine:
 $\Lambda^+ \rightarrow \Lambda^*_+ (\nu_B, B_f, \Lambda)$. Example, $\Lambda^*_+ = \frac{9(4+B)\nu_B}{4(3+2B\Lambda)}$ makes $\delta = 0$.

Solid wall:

- **Bounce-back:** $f_q(\vec{r}_b, t + 1) = \tilde{f}_{\bar{q}}(\vec{r}_b, t)$
with $\vec{c}_{\bar{q}} = -\vec{c}_q$ and $\vec{r}_b + \vec{c}_q \in \text{solid}$



For a straight channel of width H , the bounce-back closure relation reads:

$$u_x \pm \frac{1}{2}\alpha^+ \bar{\Delta}_y u_x + \frac{1}{8}\alpha^- \bar{\Delta}_y^2 u_x \Big|_{y_{\text{wall}} = \pm \frac{H}{2} \mp \frac{1}{2}} = 0$$

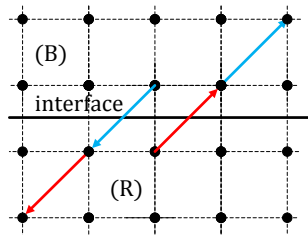
with $\alpha^+ = (1 + \delta)$ and $\alpha^- = (1 + \delta) \frac{16}{3} \Lambda$
(different coefficient values for IBF)

Interface:

- Implicit interface

$$\begin{cases} f_q(\vec{r}^{(B)}, t+1) = \tilde{f}_q(\vec{r}^{(R)}, t) \\ \tilde{f}_{\bar{q}}(\vec{r}^{(B)}, t) = f_{\bar{q}}(\vec{r}^{(R)}, t+1) \end{cases}$$

$$\text{with } \vec{r}^{(B)} = \vec{r}^{(R)} + \vec{c}_q$$



For stratified channels the steady-state closure relation for the (implicit) interface reads:

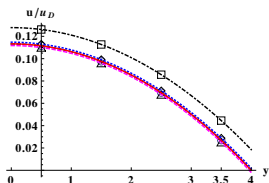
$$\|\nu_i(\bar{\Delta}_y u_x^{(i)} \pm \frac{1}{2} \bar{\Delta}_y^2 u_x^{(i)})\|_{Y_{i \mp} \frac{H}{2}} = 0, \quad \nu_i = \nu_B^{(i)} (1 + \delta_i),$$

$$\|u_x^{(i)} \pm \frac{1}{2} \alpha^+ \bar{\Delta}_y u_x^{(i)} + \frac{1}{8} \alpha^- \bar{\Delta}_y^2 u_x^{(i)}\|_{Y_{i \mp} \frac{H}{2}} = 0$$

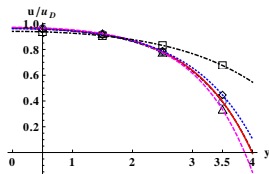
with $\alpha^+ = (1 + \delta)$ and $\alpha^- = (1 + \delta) \frac{16}{3} \Lambda$
(different coefficient values for IBF)

Bounded channel

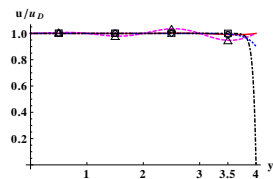
Solutions width $H = 8$ with $\Lambda = \left\{ \frac{1}{512}, \frac{3}{16}, \frac{3}{8}, 2 \right\}$



Stokes-Brinkman regime
($\sigma = 1$)



Brinkman regime ($\sigma = 8$)

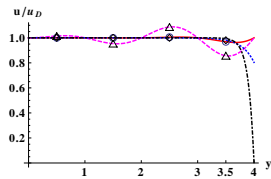
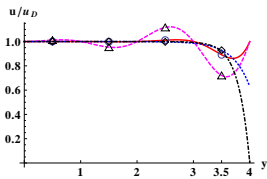
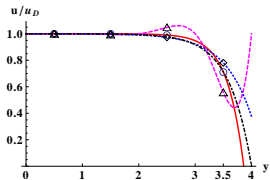


Darcy-Brinkman regime
($\sigma = 160$)

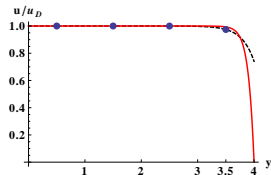
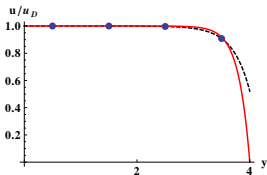
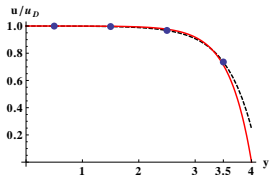
Bounded channel

Solutions width $H = 8$ with $\Lambda = \left\{ \frac{1}{512}, \frac{3}{16}, \frac{3}{8} \right\}$

BF:

Brinkman regime ($\sigma = 20$)Brinkman regime ($\sigma = 40$)Brinkman regime ($\sigma = 80$)

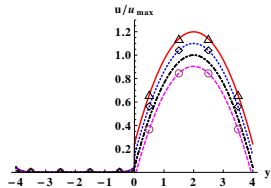
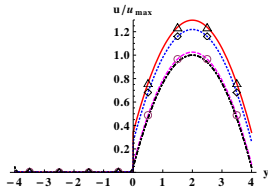
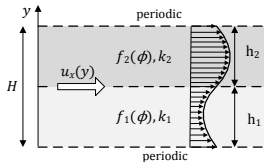
IDF:



Solutions

Unbounded channel

Solutions width $H = 8$ with $\Lambda = \left\{ \frac{1}{512}, \frac{1}{8}, \frac{3}{16} \right\}$

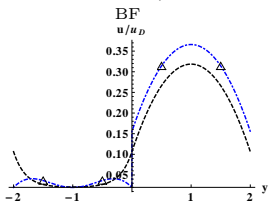


Periodic unbounded channel

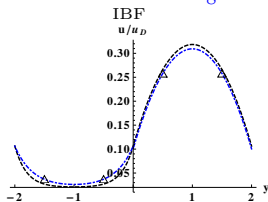
$\sigma \approx 0.26, k_2/k_1 = 10^6$ (BF)

$\sigma \approx 0.26, k_2/k_1 = 10^6$ (IBF)

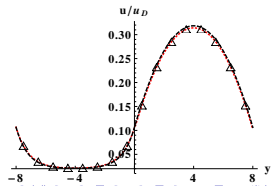
$\sigma \approx 2.8, k_2/k_1 = 10^2$:



$H = 4$ and $\Lambda = \frac{1}{8}$



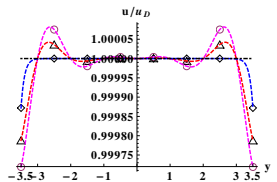
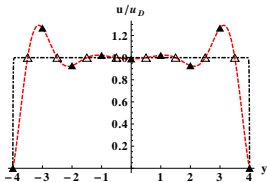
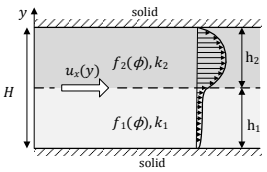
$H = 8$ and $\Lambda = \frac{1}{8}$
IBF(\approx BF)



Solutions

Bounded layered channel: FEM vs TRT (BF)

Solutions width $H = 8$ with $\Lambda = \left\{ \frac{1}{512}, \frac{3}{16}, \frac{3}{8} \right\}$



Bounded stratified channel

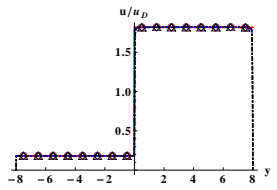
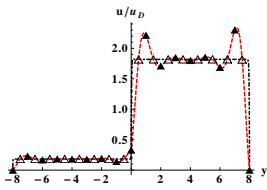
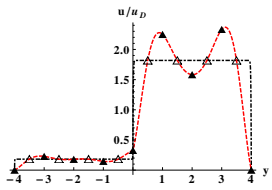
$\sigma = 10^3, k_2 = k_1$ (FEM/BF)

Zoom in: $\sigma = 10^3, k_2 = k_1$ (BF)

$H = \{8, 16\}$ and $\Lambda = \frac{1}{8}$

$\sigma = 10^3, k_2/k_1 = 10$

$H = 16$ and $\Lambda = \left\{ \frac{1}{8}, \frac{3}{16}, \frac{3}{8} \right\}$



Brinkman flow in bounded channels: boundary condition

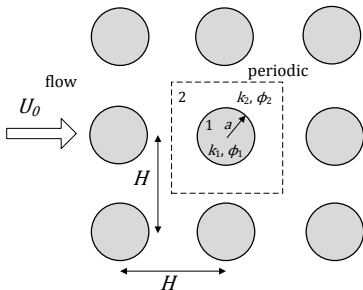
- Physical solution experiences three regimes: Stokes, Brinkman, Darcy.
- Discrete solution is controlled by bulk and boundary approximations.
- Bulk error in BF is vanished for $\Lambda = 3/8$. For $\Lambda < 3/8$ may lead to wiggles in bulk solution. Bulk error is absent by construction in IBF.
- Bounce-back boundary error is always present (already at the 1st order) for $B \neq 0$ (when $B = 0$, it is exact for $\Lambda < 3/16$).
- Bounce-back prescribes boundary implicitly. It allows smoother bulk accommodation on wall. Enforcement on wall nodes triggers oscillations, e.g. FEM.

Brinkman flow in layered channels: interface condition

- Discrete solution is controlled by bulk and interface approximations.
- Implicit interface prescription may lead to jumps in continuity conditions.
- Interface continuity is only exact for $B = 0$ (Stokes). Interface jumps increase for $B \gg 1$ (Darcy). They decrease for $\Lambda \ll 1$, but produce wiggles. Solution: IBF.

Benchmark description

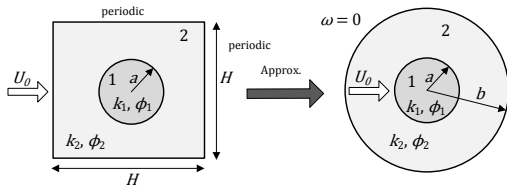
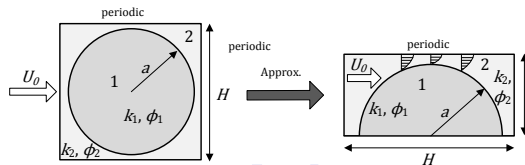
Idealized geometry:



Characteristic parameters:

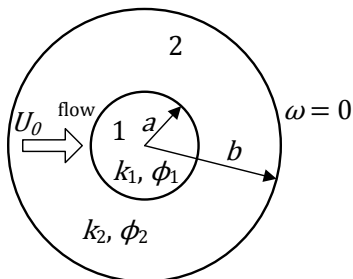
- Obstacles configuration:
Square array arrangement
- Obstacles concentration:

$$c = \frac{\pi a^2}{H^2}$$

Cell model
(dilute limit):
 $c < 1$
Lubrication theory
(high concentration limit):
 $c \sim 1$


Approximated solutions

Cell model:



General solution (Brinkman):

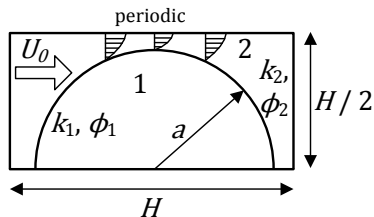
$$\psi^{(i)}(r, \theta) = \left(\frac{C_1^{(i)}}{r} + C_2^{(i)}r + C_3^{(i)}I_1(\sigma_1 r) + C_4^{(i)}K_1(\sigma_1 r) \right) \sin(\theta)$$

subject to proper interface/solid BC

Main features:

- Ratio of particle to cell volume c remains invariant
- Independent of packing arrangement (in principle requires $c \ll 1$)
- Approximation on outer BC: $\omega = 0$ (Kuwabara model)
- Polar coordinates: $(x, y) \mapsto (r, \theta)$
- Streamfunction formulation: $u_r = \frac{1}{r} \frac{\partial \psi}{\partial \theta}$ and $u_\theta = -\frac{\partial \psi}{\partial r}$

Lubrication theory:



General solution (Brinkman):

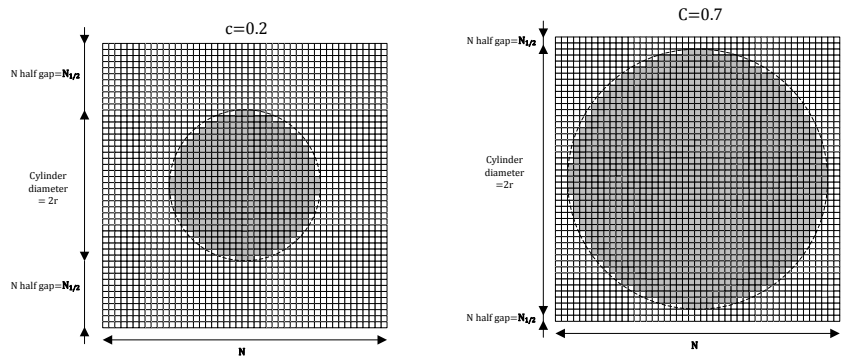
$$u_x^{(i)}(y) = -\frac{1}{\sigma_i^2} \frac{dp}{dx} + C_1^{(i)} \exp(y\sigma_i) + C_2^{(i)} \exp(-y\sigma_i)$$

subject to proper interface/solid BC

Main features:

- Ratio of particle to cell volume c remains invariant
- Depends on packing arrangement
- Approximation in bulk: flow asymptotically unidirectional (Lubrication model)
- Caution: singular behaviour when $H/2 - a \rightarrow 0$

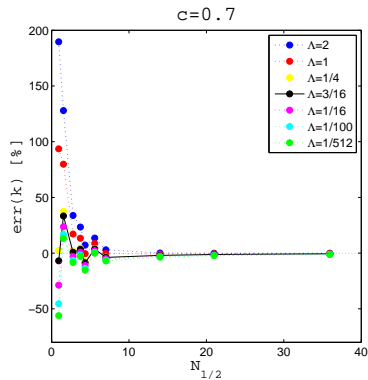
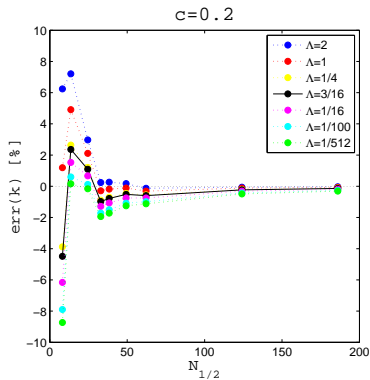
Domain discretization



Solid cylinder is discretized in a regular grid by *bounce-back* (i.e. as staircase shape), introducing a discretization error of $O(N^{-1})$

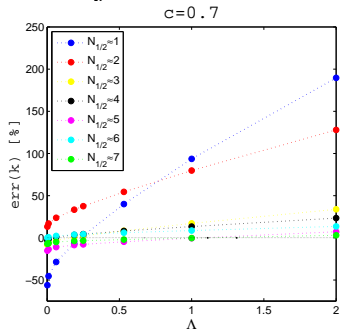
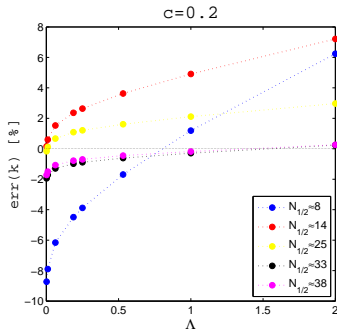
Note: Numerical solutions are evaluated for one half gap size – $N_{1/2}$

Effect of lattice resolution on accuracy



is non-monotonic and with large dependency on Λ at coarse resolutions

Effect of Λ on accuracy

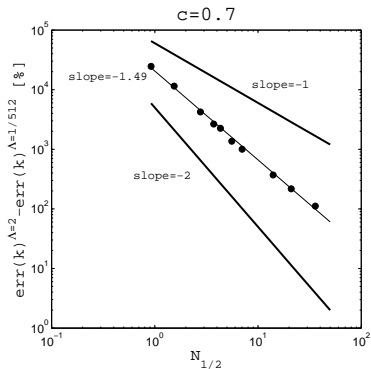
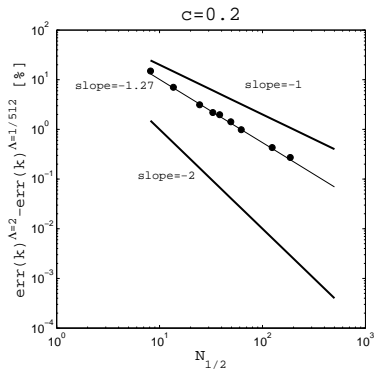


For fixed lattice resolution Λ controls Stokes solution accuracy through the location of *bounce-back* solid boundary

Remarks:

- 1 Staircase representation of cylinder reduces its true hydraulic diameter \Rightarrow makes permeability solution converge to a smaller value
- 2 Large Λ reduces hydraulic diameter of cylinder \Rightarrow under-estimates permeability at fixed grid resolution, i.e. $\left. \frac{\partial \text{err}(k)}{\partial \Lambda} \right|_N > 0$

Effect of lattice resolution on accuracy



becomes monotonic taking difference between any two Λ solutions

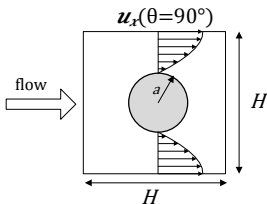
- Spatial convergence rate is between 1st- and 2nd-order

Porous flow around solid cylinder

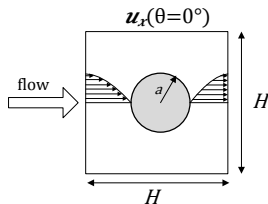
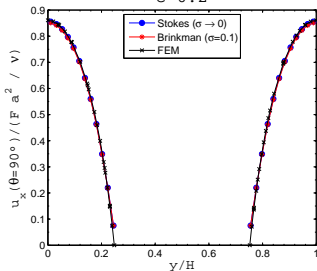
Stokes regime



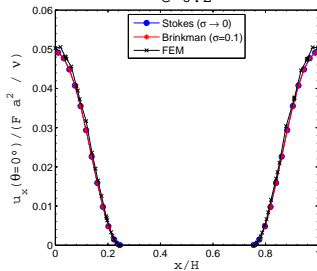
$$\vec{\nabla} p = \Delta \vec{u} - \underbrace{\sigma^2 \vec{u}}_{\sigma \rightarrow 0}$$



c=0.2



c=0.2

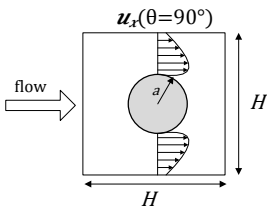
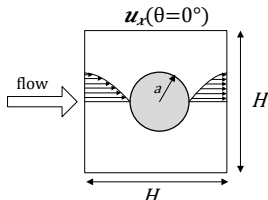
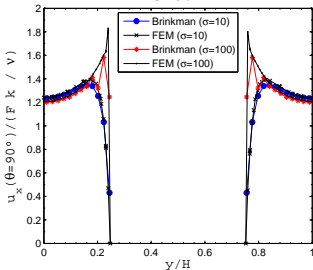
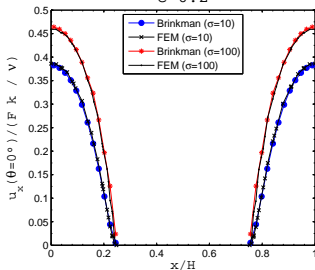


Porous flow around solid cylinder

Brinkman regime



$$\vec{\nabla} p = \Delta \vec{u} - \underbrace{\sigma^2 \vec{u}}_{\sigma \sim O(1)}$$

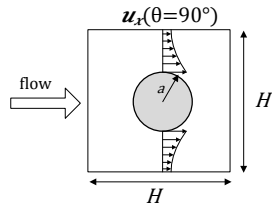
 $c=0.2$  $c=0.2$ 

Porous flow around solid cylinder

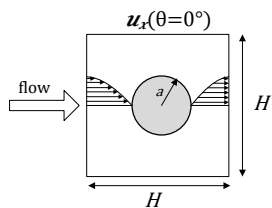
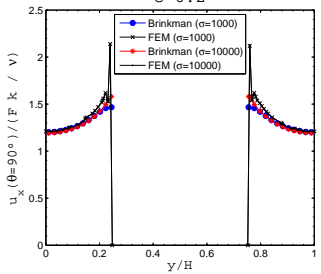
Darcy regime



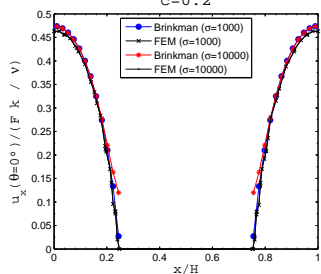
$$\vec{\nabla} p = \Delta \vec{u} - \underbrace{\sigma^2 \vec{u}}_{\sigma \rightarrow \infty}$$



$c=0.2$

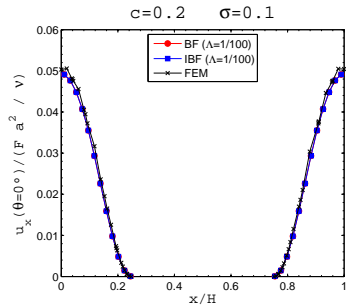
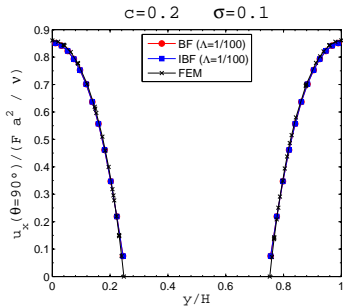
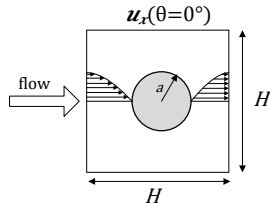
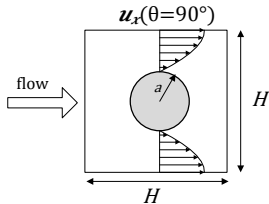


$c=0.2$

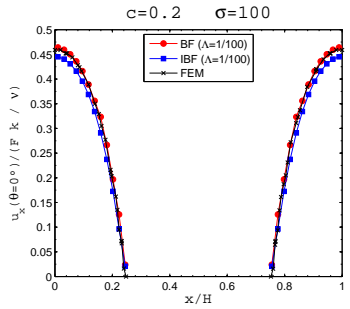
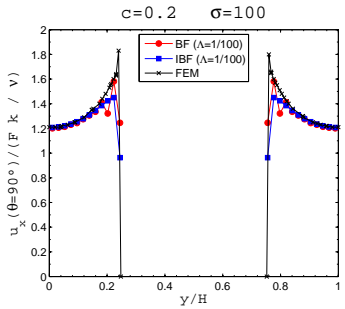
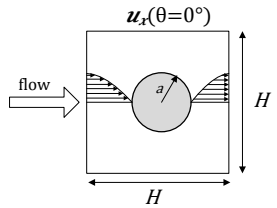
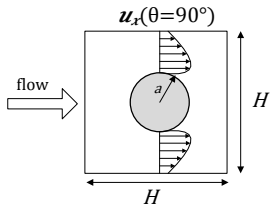


Porous flow around solid cylinder

Stokes regime (with IBF)

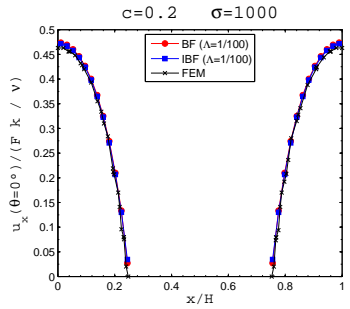
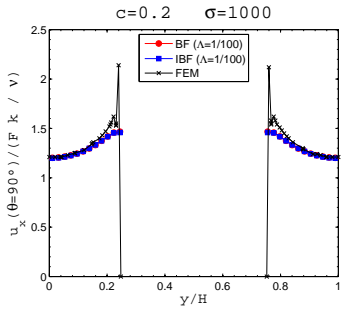
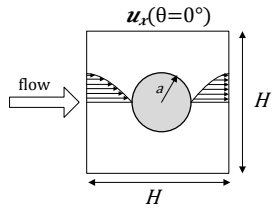
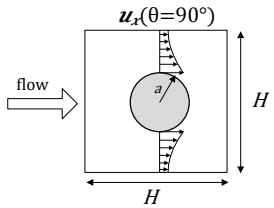


Brinkman regime (with IBF)



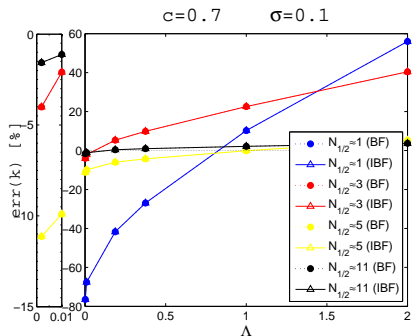
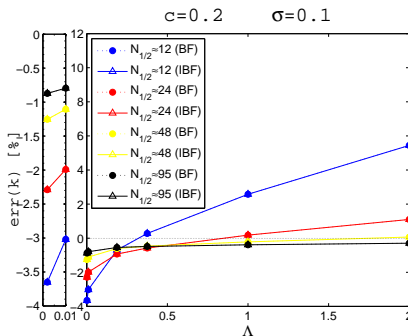
Porous flow around solid cylinder

Darcy regime (with IBF)



Effect of Λ on accuracy

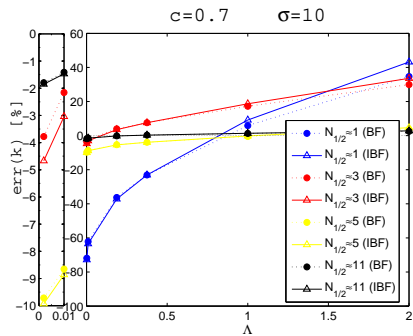
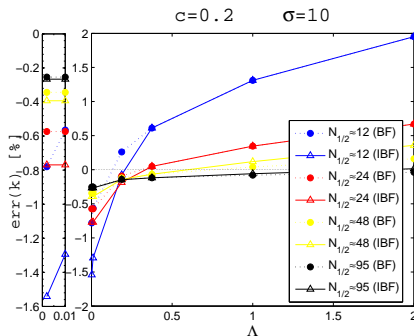
Stokes regime



Essentially similar to TRT Stokes solver $\Rightarrow \Lambda$ controls the accuracy through the location of *bounce-back* solid boundary

Effect of Λ on accuracy

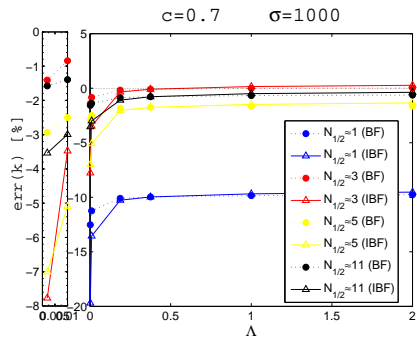
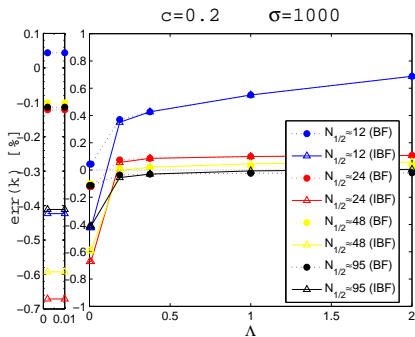
Brinkman regime



Brinkman correction (in bulk and boundary) now plays a role
 \Rightarrow smaller influence of Λ over accuracy (compared to Stokes)

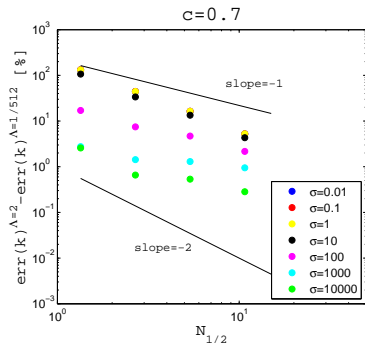
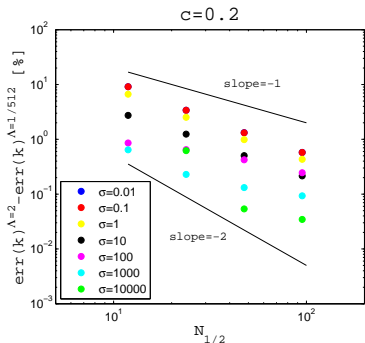
Effect of Λ on accuracy

Darcy regime



Accuracy becomes independent of Λ except at small Λ values

Effect of lattice resolution on accuracy



$\forall \sigma$ spatial convergence rate between 1st- and 2nd-order

(Data shown for BF model)

Stokes flow around solid cylinder

- Role of Λ controls the location of the bounce-back solid boundary (by varying the size of cylinder)
- Dependency on Λ is larger at coarser lattice resolutions
- Dependency on lattice resolution indicates spatial convergence rate between 1st- and 2nd-order

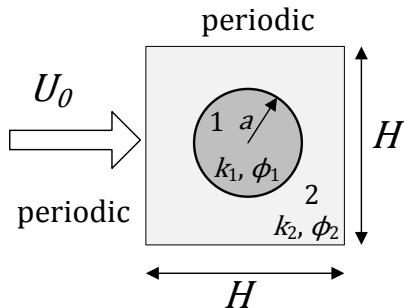
Porous flow around solid cylinder

- 3 physical regimes: Stokes $\sigma \ll 1$, Brinkman $\sigma \sim O(1)$, Darcy $\sigma \gg 1$
- Stokes regime: role of Λ controls the location of the bounce-back solid boundary \Rightarrow accuracy is worst and larger dependency on Λ
- Brinkman regime: role of Λ controls both bulk and boundaries errors (Brinkman correction). Better accuracy for k . Yet, velocity solutions may experience wiggles \Leftarrow IBF corrects them ☺
- Darcy regime: role of Λ tends to cease, except at small Λ values
- Effect of lattice resolution indicates spatial convergence rate between 1st- and 2nd-order $\forall \sigma$ regimes

Two physical problems to distinguish from:

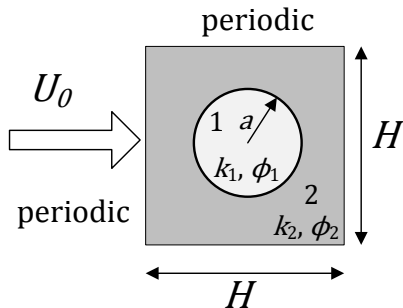
1) Porous cylinder is less permeable than outside porous medium

$$\frac{k_1}{k_2} < 1$$



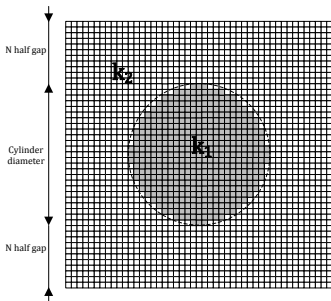
2) Porous cylinder is more permeable than outside porous medium

$$\frac{k_1}{k_2} > 1$$

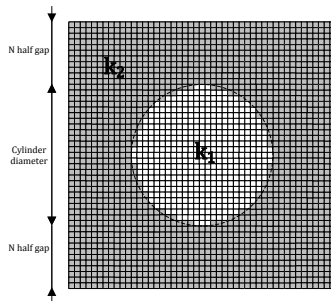


In both cases, **interface** continuity conditions are set *implicitly* and approximate a *staircase* cylinder

$$\frac{k_1}{k_2} < 1$$



$$\frac{k_1}{k_2} > 1$$



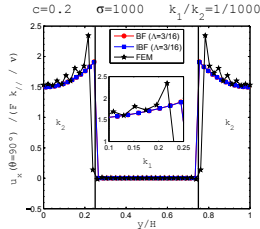
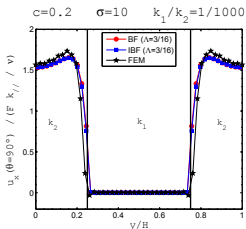
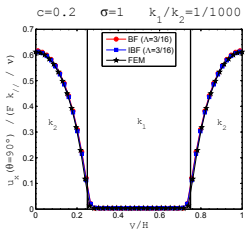
Porous flow across porous cylinder $k_1 \ll k_2$

$u_x(y)$ at vertical ($\theta = 90^\circ$) midplane for $\frac{k_1}{k_2} = \frac{1}{1000}$ and $c = 0.2$

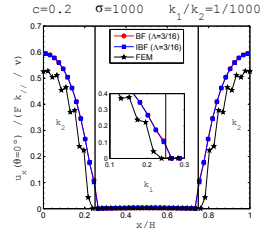
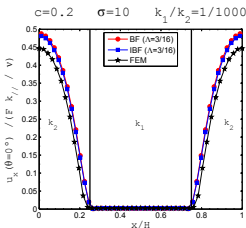
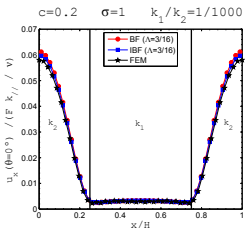
“Stokes-type flow”

“Brinkman-type flow”

“Darcy-type flow”



$u_x(x)$ at horizontal ($\theta = 0^\circ$) midplane for $\frac{k_1}{k_2} = \frac{1}{1000}$ and $c = 0.2$

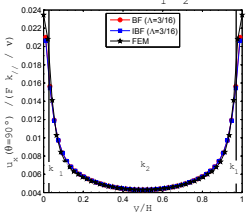


Porous flow across porous cylinder $k_1 \ll k_2$

$u_x(y)$ at vertical ($\theta = 90^\circ$) midplane for $\frac{k_1}{k_2} = \frac{1}{1000}$ and $c = 0.7$

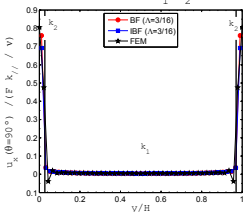
“Stokes-type flow”

$c=0.7 \quad \sigma=1 \quad k_1/k_2=1/1000$



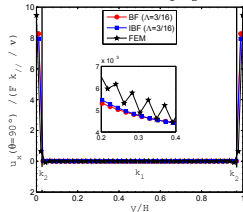
“Brinkman-type flow”

$c=0.7 \quad \sigma=10 \quad k_1/k_2=1/1000$



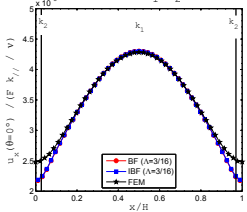
“Darcy-type flow”

$c=0.7 \quad \sigma=1000 \quad k_1/k_2=1/1000$

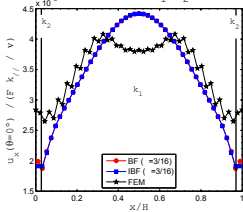


$u_x(x)$ at horizontal ($\theta = 0^\circ$) midplane for $\frac{k_1}{k_2} = \frac{1}{1000}$ and $c = 0.7$

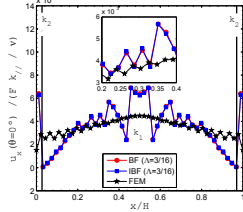
$c=0.7 \quad \sigma=1 \quad k_1/k_2=1/1000$



$c=0.7 \quad \sigma=10 \quad k_1/k_2=1/1000$

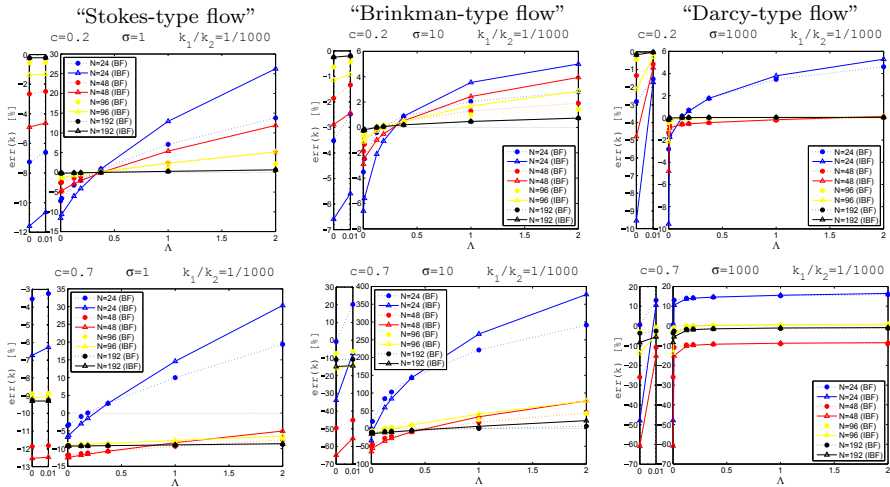


$c=0.7 \quad \sigma=1000 \quad k_1/k_2=1/1000$



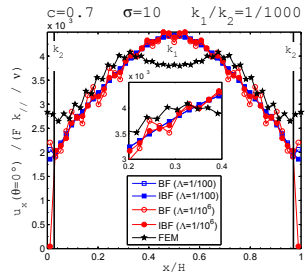
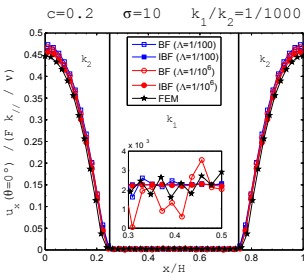
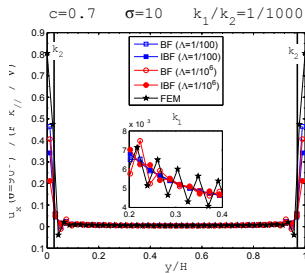
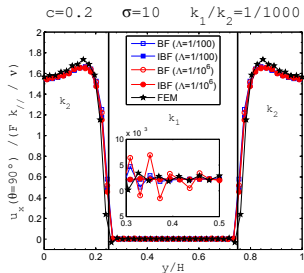
Porous flow across porous cylinder $k_1 \ll k_2$

Effect of Λ on accuracy for $\frac{k_1}{k_2} = \frac{1}{1000}$

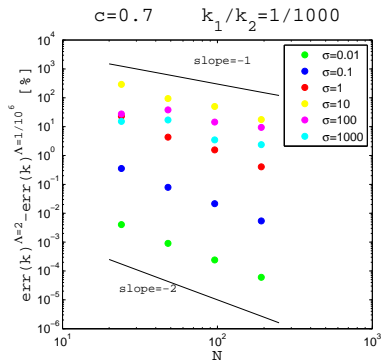
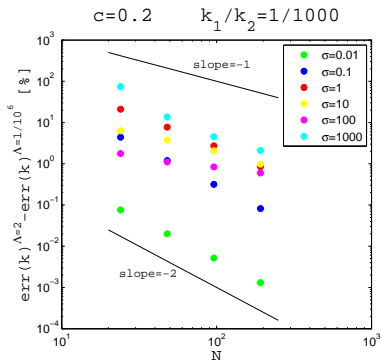


Porous flow across porous cylinder $k_1 \ll k_2$

Effect of **IBF** on $u_x(y)$ and $u_x(x)$ for $\frac{k_1}{k_2} = \frac{1}{1000}$



Effect of lattice resolution on accuracy for $\frac{k_1}{k_2} = \frac{1}{1000}$



$\forall \sigma$ spatial convergence rate between 1st- and 2nd-order

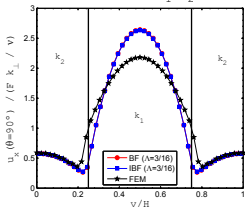
(Data shown for BF model)

Porous flow across porous cylinder $k_1 \gg k_2$

$u_x(y)$ at vertical ($\theta = 90^\circ$) midplane for $\frac{k_1}{k_2} = 1000$ and $c = 0.2$

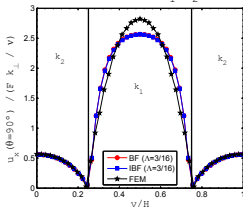
“Stokes-type flow”

$c=0.2 \quad \sigma=1 \quad k_1/k_2=1000$



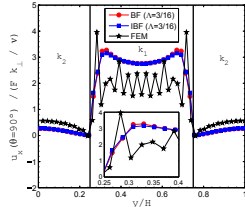
“Brinkman-type flow”

$c=0.2 \quad \sigma=10 \quad k_1/k_2=1000$



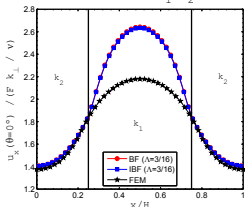
“Darcy-type flow”

$c=0.2 \quad \sigma=1000 \quad k_1/k_2=1000$

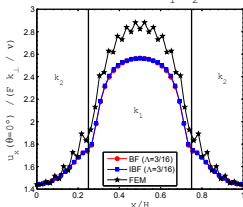


$u_x(x)$ at horizontal ($\theta = 0^\circ$) midplane for $\frac{k_1}{k_2} = 1000$ and $c = 0.2$

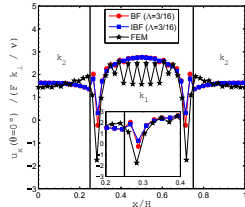
$c=0.2 \quad \sigma=1 \quad k_1/k_2=1000$



$c=0.2 \quad \sigma=10 \quad k_1/k_2=1000$



$c=0.2 \quad \sigma=1000 \quad k_1/k_2=1000$

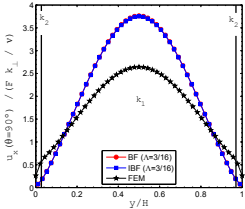


Porous flow across porous cylinder $k_1 \gg k_2$

$u_x(y)$ at vertical ($\theta = 90^\circ$) midplane for $\frac{k_1}{k_2} = 1000$ and $c = 0.7$

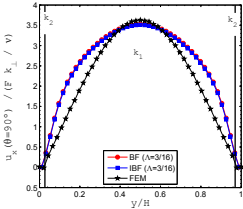
“Stokes-type flow”

$c=0.7 \quad \sigma=1 \quad k_1/k_2=1000$



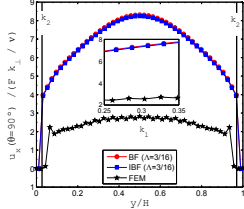
“Brinkman-type flow”

$c=0.7 \quad \sigma=10 \quad k_1/k_2=1000$



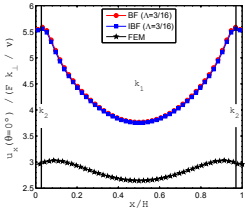
“Darcy-type flow”

$c=0.7 \quad \sigma=1000 \quad k_1/k_2=1000$

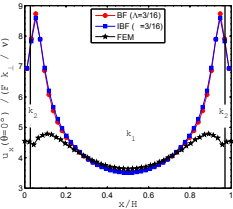


$u_x(x)$ at horizontal ($\theta = 0^\circ$) midplane for $\frac{k_1}{k_2} = 1000$ and $c = 0.7$

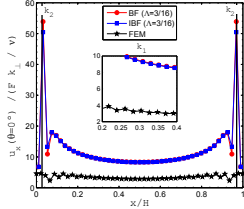
$c=0.7 \quad \sigma=1 \quad k_1/k_2=1000$



$c=0.7 \quad \sigma=10 \quad k_1/k_2=1000$

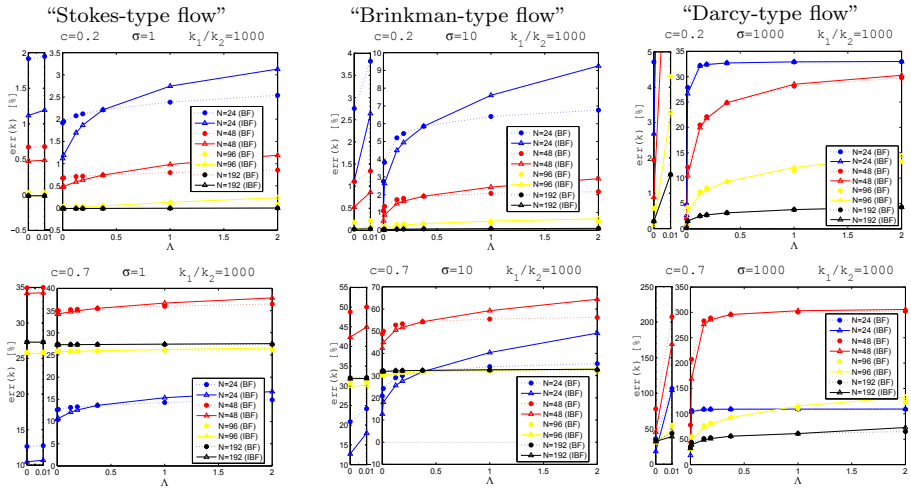


$c=0.7 \quad \sigma=1000 \quad k_1/k_2=1000$

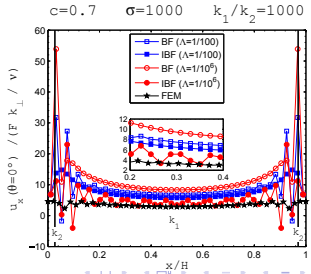
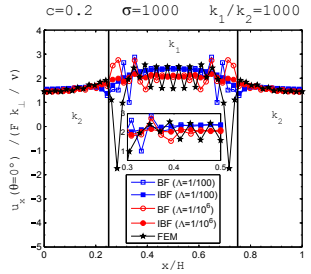
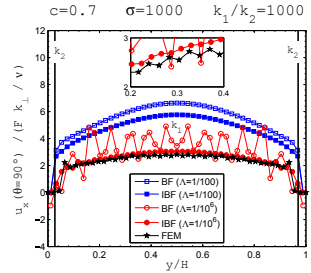
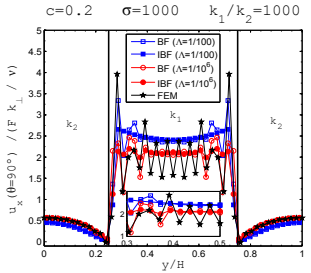


Porous flow across porous cylinder $k_1 \gg k_2$

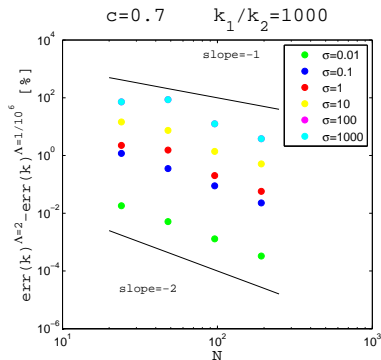
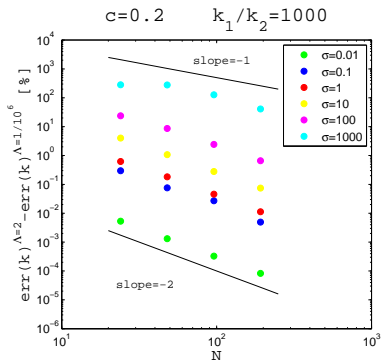
Effect of Λ on accuracy for $\frac{k_1}{k_2} = 1000$



Effect of IBF on $u_x(y)$ and $u_x(x)$ for $\frac{k_1}{k_2} = 1000$



Effect of lattice resolution on accuracy for $\frac{k_1}{k_2} = 1000$



$\forall \sigma$ spatial convergence rate between 1st- and 2nd-order

(Data shown for BF model)

Biporous medium: $k_1 \ll k_2$

- Solutions behave, approximately, as case of Brinkman flow around solid cylinder.
- However, with interface playing the role of boundary we recover larger errors (particularly in Brinkman regime).
- TRT velocity solutions are *over-estimated*, except for small Λ
- Small Λ values lead to wiggles velocity solution profiles. They are partially corrected by IBF
- Dependency on **lattice resolution** indicates spatial convergence rate between 1st- and 2nd-order

Biporous medium: $k_1 \gg k_2$

- TRT velocity solutions are *significantly over-estimated* in Darcy regime. Solution requires use of small Λ
- However, small Λ values produce *strong* wiggles in velocity profiles. They are successfully corrected by IBF
- Dependency on **lattice resolution** indicates spatial convergence rate between 1st- and 2nd-order